

slightly acute angle. A large tube three fourths inch in diameter is best. The amalgam is broken into pieces small enough to be dropped into the closed end where it is then heated, the fumes condensing in the long open end of the tube. The gold can be annealed by heating the tube to redness after all mercury is driven off.

A retort for treating a few ounces at a time can be made cheaply of 3/8-inch pipe, pipe connections, and a large grease cup. The lower and open end of the 3/8-inch pipe is inclosed in a larger pipe. Cooling water is poured through the space between the two pipes from an open connection in the top of the outer one. The charge of amalgam is placed in the grease-cup cover which is then screwed into place; graphite lubricant is placed on the threads to make a tight joint. Heat is applied to the grease cup, and the quicksilver is condensed in the lower end of the pipe. The method of using and the general arrangement of the device are similar to those of the next retort described.

The typical quicksilver retort for placer mines (fig. 15, G and D) is a cast-iron pot with a tight-fitting cover in which a hole is tapped to accommodate the condenser pipe. The capacities of such retorts range from a few to 200 pounds of amalgam, or about a quarter pint to 2 gallons. They are listed in chemical-supply catalogs at prices ranging from \$4 to \$30, not including the condensers. The condenser commonly used with this type of retort is an iron pipe 3 or 4 feet long leading from the hole in the retort cover at a downward angle of 20 to 30°; it is encased for most of its length in a considerably larger pipe through which cooling water is circulated. When heat is applied to the charged retort the mercury vapor enters the condenser pipe where it cools and condenses; it trickles down the pipe into a vessel placed under the open end of the pipe. In the treatment of a large amount of amalgam the temperature of the pipe might be raised to a point where some of the vapor would escape; therefore, a cooling device is necessary.

The retort may be heated over a large bunsen burner, by a gasoline blow torch, in a forge, or in one of several types of furnaces built for the purpose. Very high temperatures are unnecessary, and a wood fire is considered better than a coal fire. The flame should cover as much of the retort as possible.

A rigid, strong stand for the retort and condenser (fig. 15.A) should be constructed if the apparatus is to be used regularly.

The retort should be coated on the inside with chalk, or painted with a thin paste of chalk, clay, mill slimes, or a mixture of fire clay and graphite and thoroughly dried before putting in the charge. This prevents the gold from sticking to the iron, which sometimes causes trouble. A lining of paper serves the same purpose but tends to form an objectionable deposit in the condenser pipe.

The retort should not be filled over two thirds full of amalgam (a third or half full when retorting liquid mercury), otherwise there is danger of some of the contents boiling over into the condenser tube. The amalgam is broken into pieces and piled loosely. Then the cover is put on and clamped tightly with the wedge or thumbscrew provided, first making sure that the attached condenser pipe is clean and free of obstructions. The ground joint between the cover and body of the retort is seldom tight enough to prevent leakage and should be luted with clay or some sealing compound. One satisfactory cement is made readily by moistening a mixture of ground asbestos and litharge (red lead) with glycerin.

A low heat is applied at first, then after 10 or 15 minutes the temperature is increased just enough to start the mercury vaporizing and condensing. Too rapid heating harms the retort, and only enough heat should be used to maintain a steady trickle of quicksilver from the condenser. When no more mercury appears the temperature should be increased for a few minutes to ~~reheat~~ drive the last of the quicksilver out of the retort; then the fire should be withdrawn from the retort and the latter allowed to cool. Some mercury vapor always remains in the retort, and the operator should take care not to breathe these fumes upon taking off the cover.

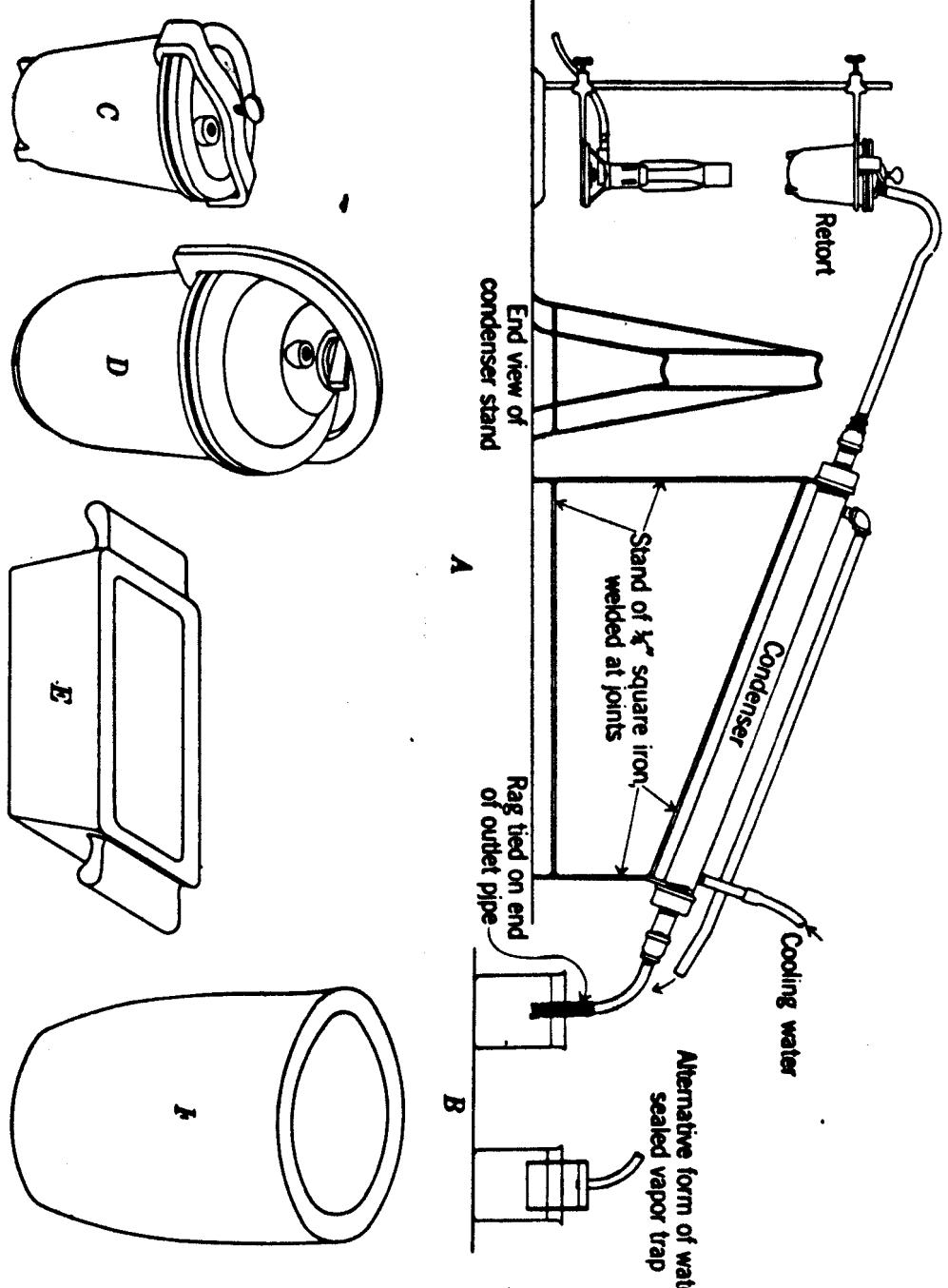


Figure 15.—Apparatus for retorting amalgam and quicksilver: A, Amalgam retort; B, Nevada-type retort; C, set-up of small retort; D, water-sealed vapor trap; E, graphite crucible; F, bullion mould.

46 Louis, Henry, A Handbook of Cold Milling; London, 1894, p. 386.
47 Patients, C. G., Method and Costs of Dredging Artificial Rivers Graves at Laonche Plaza, Asador County, Calif.; Int. Crit.

In several localities in the western States sulfide concentrations from placer mining are likely to contain platinum or its associated metals in sufficient quantities to be of economic interest. The separation of these minerals from gold is difficult. Their specific gravity is too near that of gold to permit a separation by panning. Coarse platinum particles can be picked out of the gold by hand, but most placer platinum is exceedingly fine. Although platinum does not amalgamate, it looks like an amalgamate, and though platinum separates by treatment with chemicals; thus it is possible to separate successively the gold and platinum from the concentrates.

The dredging company in California which recovers platinum metals uses the following clean-up procedure:⁴⁷

In cleaning up, the riffles are removed from the sluices, starting at the head end, carefully washing them off and washing the sluice down with water from a hose. This washes away the light sand and concentrates the amalgam and heavy sands, which are carefully scooped up into buckets and carried to a "long ton" tank. In the long ton most of the mercury and amalgam and some gold rather treatment. In the long ton most of the mercury and amalgam and some

SEPARATION OF PLATINUM-GROUP METALS FROM GOLD

If the volume of the receiver pipe is very small compared with that of the condenser pipe and if the discharge pipe is barely submerged the danger is avoided, as any large rise of water in the pipe would lower the water surface enough to break the suction. At some proper distance from the end of the condenser pipe is a large sheet-iron cylinder, a few inches in diameter, open at the lower end, which may be placed 2 or 3 inches into the water in a recessed hole of only slight depth. Larger diameter, thus making a good-water seal yet avoiding the danger of explosion. A laboratory adaptation of this device is shown in figure 15,B.

The simplest method is that recommended by Louis⁴; it consists merely of tying a piece of cloth such as canvas or burlap around the end of the condenser pipe and letting it dip in the water 2 or 3 inches below, forming a damp filter which will condense any escaping vapor and not be tight enough to permit water to be sucked into the rotor. This device is shown in figure 15,A.

Large gold mines use cylindrical rotors, usually set horizontally in specially built furnaces. Such installations probably would be needed in place of burning only by large dredging companies. The operation is similar to that of a hot rotor, except that the amalgam usually is placed in several small iron trays, rather than on the floor of the rotor, while the condenser and charged through a door of removable cover at one end of the rotor, while the condenser and the amalgam are heated by gas or oil.

The likelihood of dangerous amounts of mercury vapor passing through a long cold pipe without condensing is very small. However, if much amalgam is to be retorted, or if the operation is of daily or frequent occurrence, it usually is desirable to provide some form of water seal at the end of the condenser tube to prevent the escape of such fumes. Many mines have followed the dangerous practice of submerging the end of the condenser pipe in the bucket of water used to receive the condensed mercury. This should not be done, as a slight flooding of the report would cause water to be sucked into the pipe, and if the water reached the bottom of the condenser tube it would be impossible to remove the amalgam.

The same general types of derricks and winches are used as in ground-sludging, which has been described in a previous paper.¹⁸

Derricks and Winches

Adapted from table in catalog of Joshua Hendy Iron Works, San Francisco, Calif.

Class of derrick	Effective head, feet				100				200				300				400			
	Cubits	Nozzles	feet per minute	cubits	Cubits	Nozzles	feet per minute	cubits	Cubits	Nozzles	feet per minute	cubits	Cubits	Nozzles	feet per minute	cubits	Cubits	Nozzles	feet per minute	
0	1 1/8	0.6	0.8	0.8	0.8	32	0.8	32	1.2	47	1.2	0.8	33	1.6	0.8	33	1.2	109	3.1	125
1	2	1.6	1.8	1.8	1.8	63	1.8	63	2.2	47	2.2	1.8	63	2.2	1.8	63	2.2	120	3.1	125
2	3	3.0	3.0	3.0	3.0	120	3.0	120	4.3	227	4.3	3.0	123	4.3	3.0	123	4.3	110	3.1	125
3	4	3.5	3.5	3.5	3.5	133	3.5	133	4.7	227	4.7	3.5	127	4.7	3.5	127	4.7	110	3.1	125
4	4	4.0	4.0	4.0	4.0	148	4.0	148	5.0	240	5.0	4.0	200	5.0	4.0	200	5.0	110	3.1	125
5	5	4.5	4.5	4.5	4.5	153	4.5	153	5.6	245	5.6	4.5	245	5.6	4.5	245	5.6	110	3.1	125
6	6	5.0	5.0	5.0	5.0	159	5.0	159	6.6	248	6.6	5.0	248	6.6	5.0	248	6.6	110	3.1	125
7	7	5.5	5.5	5.5	5.5	164	5.5	164	7.3	253	7.3	5.5	200	7.3	5.5	200	7.3	110	3.1	125
8	8	6.0	6.0	6.0	6.0	169	6.0	169	8.0	257	8.0	6.0	200	8.0	6.0	200	8.0	110	3.1	125
9	9	6.5	6.5	6.5	6.5	174	6.5	174	8.7	262	8.7	6.5	200	8.7	6.5	200	8.7	110	3.1	125
10	10	7.0	7.0	7.0	7.0	179	7.0	179	9.4	267	9.4	7.0	200	9.4	7.0	200	9.4	110	3.1	125
11	11	7.5	7.5	7.5	7.5	184	7.5	184	10.1	272	10.1	7.5	200	10.1	7.5	200	10.1	110	3.1	125
12	12	8.0	8.0	8.0	8.0	189	8.0	189	10.8	277	10.8	8.0	200	10.8	8.0	200	10.8	110	3.1	125
13	13	8.5	8.5	8.5	8.5	194	8.5	194	11.5	282	11.5	8.5	200	11.5	8.5	200	11.5	110	3.1	125
14	14	9.0	9.0	9.0	9.0	199	9.0	199	12.2	287	12.2	9.0	200	12.2	9.0	200	12.2	110	3.1	125
15	15	9.5	9.5	9.5	9.5	204	9.5	204	12.9	292	12.9	9.5	200	12.9	9.5	200	12.9	110	3.1	125
16	16	10.0	10.0	10.0	10.0	209	10.0	209	13.6	297	13.6	10.0	200	13.6	10.0	200	13.6	110	3.1	125
17	17	10.5	10.5	10.5	10.5	214	10.5	214	14.3	302	14.3	10.5	200	14.3	10.5	200	14.3	110	3.1	125
18	18	11.0	11.0	11.0	11.0	219	11.0	219	15.0	307	15.0	11.0	200	15.0	11.0	200	15.0	110	3.1	125
19	19	11.5	11.5	11.5	11.5	224	11.5	224	15.7	312	15.7	11.5	200	15.7	11.5	200	15.7	110	3.1	125
20	20	12.0	12.0	12.0	12.0	229	12.0	229	16.4	317	16.4	12.0	200	16.4	12.0	200	16.4	110	3.1	125
21	21	12.5	12.5	12.5	12.5	234	12.5	234	17.1	322	17.1	12.5	200	17.1	12.5	200	17.1	110	3.1	125
22	22	13.0	13.0	13.0	13.0	239	13.0	239	17.8	327	17.8	13.0	200	17.8	13.0	200	17.8	110	3.1	125
23	23	13.5	13.5	13.5	13.5	244	13.5	244	18.5	332	18.5	13.5	200	18.5	13.5	200	18.5	110	3.1	125
24	24	14.0	14.0	14.0	14.0	249	14.0	249	19.2	337	19.2	14.0	200	19.2	14.0	200	19.2	110	3.1	125
25	25	14.5	14.5	14.5	14.5	254	14.5	254	19.9	342	19.9	14.5	200	19.9	14.5	200	19.9	110	3.1	125
26	26	15.0	15.0	15.0	15.0	259	15.0	259	20.6	347	20.6	15.0	200	20.6	15.0	200	20.6	110	3.1	125
27	27	15.5	15.5	15.5	15.5	264	15.5	264	21.3	352	21.3	15.5	200	21.3	15.5	200	21.3	110	3.1	125
28	28	16.0	16.0	16.0	16.0	269	16.0	269	22.0	357	22.0	16.0	200	22.0	16.0	200	22.0	110	3.1	125
29	29	16.5	16.5	16.5	16.5	274	16.5	274	22.7	362	22.7	16.5	200	22.7	16.5	200	22.7	110	3.1	125
30	30	17.0	17.0	17.0	17.0	279	17.0	279	23.4	367	23.4	17.0	200	23.4	17.0	200	23.4	110	3.1	125
31	31	17.5	17.5	17.5	17.5	284	17.5	284	24.1	372	24.1	17.5	200	24.1	17.5	200	24.1	110	3.1	125
32	32	18.0	18.0	18.0	18.0	289	18.0	289	24.8	377	24.8	18.0	200	24.8	18.0	200	24.8	110	3.1	125
33	33	18.5	18.5	18.5	18.5	294	18.5	294	25.5	382	25.5	18.5	200	25.5	18.5	200	25.5	110	3.1	125
34	34	19.0	19.0	19.0	19.0	299	19.0	299	26.2	387	26.2	19.0	200	26.2	19.0	200	26.2	110	3.1	125
35	35	19.5	19.5	19.5	19.5	304	19.5	304	26.9	392	26.9	19.5	200	26.9	19.5	200	26.9	110	3.1	125
36	36	20.0	20.0	20.0	20.0	309	20.0	309	27.6	397	27.6	20.0	200	27.6	20.0	200	27.6	110	3.1	125
37	37	20.5	20.5	20.5	20.5	314	20.5	314	28.3	402	28.3	20.5	200	28.3	20.5	200	28.3	110	3.1	125
38	38	21.0	21.0	21.0	21.0	319	21.0	319	29.0	407	29.0	21.0	200	29.0	21.0	200	29.0	110	3.1	125
39	39	21.5	21.5	21.5	21.5	324	21.5	324	29.7	412	29.7	21.5	200	29.7	21.5	200	29.7	110	3.1	125
40	40	22.0	22.0	22.0	22.0	329	22.0	329	30.4	417	30.4	22.0	200	30.4	22.0	200	30.4	110	3.1	125

TABLE 7. - Flow of water through nozzle.

To convert cubic feet to gallons multiply by 7.48.

cu. ft. = cu. in. \times 7.48

0.94 (usually taken as 0.9, which makes all lower).

G = coefficient of discharge ranging from 0.8 to 1.0.

H = effective head at nozzle (feet).

A = area of nozzle (square feet).

Q = cubic feet per second.

where

$$Q = \frac{8CA}{\sqrt{H}}$$

I.C.6787.